## GUJARAT TECHNOLOGICAL UNIVERSITY <br> BE - SEMESTER- III (New) EXAMINATION - WINTER 2019

Subject Code: 3133606
Date: 26/11/2019

## Subject Name: Fundamentals of Material \& Energy Balance Calculations <br> Time: 02:30 PM TO 05:00 PM <br> Total Marks: 70 Instructions:

1. Attempt all questions.
2. Make suitable assumptions wherever necessary.
3. Figures to the right indicate full marks.

## Marks

Q. 1 (a) Discuss Proximate and Ultimate analysis of coal.
(b) Give Classification of material balance problems and explain it briefly.
(c) A natural gas has the following composition on mole basis: $\mathrm{CH}_{4}=84 \%$,
$\mathrm{C}_{2} \mathrm{H}_{4}=13 \%$ and $\mathrm{N}_{2}=3 \%$
Calculate the heat added to heat 10 kmol of natural gas from 298 K to 523 K using heat capacity dat given below:

$$
\mathrm{Cp}=\mathrm{a}+\mathrm{bT}+\mathrm{cT}^{2}+\mathrm{dT}^{3} \mathrm{~kJ} /(\mathrm{kmol} . \mathrm{K})
$$

| Gas | a | $\mathrm{b} \times 10^{3}$ | $\mathrm{c} \times 10^{6}$ | $\mathrm{~d} \times 10^{9}$ |
| :---: | :---: | :---: | :---: | :---: |
| $\mathrm{CH}_{4}$ | 19.2494 | 52.1135 | 11.973 | -11.3173 |
| $\mathrm{C}_{2} \mathrm{H}_{6}$ | 5.4129 | 178.0872 | -67.3749 | 8.7147 |
| $\mathrm{~N}_{2}$ | 29.5909 | -5.141 | 13.1829 | -4.968 |

Q. 2 (a) A gas containing $25 \% \mathrm{CO}, 5 \% \mathrm{CO}_{2}, 2 \% \mathrm{O}_{2}$ and the rest is $\mathrm{N}_{2}$ is burnt with $20 \%$ excess air. If the conversion is $80 \%$ complete, calculate the composition by volume of the flue gases considering the given compositions of gas to be on mole basis.
(b) Limestone mixed with coke is being burnt in a kiln. An average analysis of the limestone is $\mathrm{CaCO}_{3}=84.5 \%, \mathrm{MgCO}_{3}=11.5 \%$ and the rest is inerts. The coke contains $76 \%$ carbon $21 \%$ ash and $3 \%$ moisture. The calcination of $\mathrm{CaCO}_{3}$ is only $95 \%$ complete and that of $\mathrm{MgCO}_{3}$ is $90 \%$. The carbon in the coke is completely burnt to $\mathrm{CO}_{2}$. The kiln is fed with one kg of coke per 5 kg of limestone. Calculate the weight percent of CaO in the product leaving the kiln. Assume that the moisture in the feed is completely vaporized.
(c) Pure methane is heated from 303.15 K to 523.15 K at atmospheric pressure. Calculate the heat added per kmol methane, using date given below:

| a | $\mathrm{b} \times 10^{3}$ | $\mathrm{c} \times 10^{6}$ | $\mathrm{~d} \times 10^{9}$ |
| :---: | :---: | :---: | :---: |
| 19.2494 | 52.1135 | 11.973 | -11.3173 |

## OR

 $3 \mathrm{CaSO}_{4(\mathrm{~s})}+\mathrm{SiO}_{2(\mathrm{~s})} \quad 3 \mathrm{CaO} . \mathrm{SiO}_{2(\mathrm{~s})}+\mathrm{SO}_{2(\mathrm{~g})}+3 / 2 \mathrm{O}_{2(\mathrm{~g})}$

| Component | $\Delta \mathbf{H}^{\mathbf{0}} \mathbf{f}, \mathbf{k J / m o l}$ at $\mathbf{2 9 8 . 1 5 ~ K}$ <br> $\left(\mathbf{2 5}^{\mathbf{0}} \mathbf{C}\right)$ |
| :---: | :---: |
| $\mathrm{CaSO}_{4(\mathrm{~s})}$ | -1432.7 |
| $\mathrm{SiO}_{2(\mathrm{~s})}$ | -903.5 |
| $3{\mathrm{CaO} . \mathrm{SiO}_{2(\mathrm{~s})}}^{-2879}$ |  |
| $\mathrm{SO}_{2(\mathrm{~g})}$ | -296.81 |
| $\mathrm{O}_{2(\mathrm{~g})}$ | 0.0 |

Q. 3 (a) Define following terms (a) Yield (b) limiting reactant and (c) Molality ..... 03
(b) What are the methods of expressing the composition of mixtures and ..... 04solutions?
(c) The waste acid from a nitrating process containing $20 \% \mathrm{HNO}_{3}, 55 \% \mathrm{H}_{2} \mathrm{SO}_{4}$and $25 \% \mathrm{H}_{2} \mathrm{O}$ by weight is to be concentrated by addition of concentratedsulphuric acid containing $90 \% \mathrm{HNO}_{3}$ to get desired mixed acid containing$26 \% \mathrm{HNO}_{3}$ and $60 \% \mathrm{H}_{2} \mathrm{SO}_{4}$. Calculate the quantities of waste andconcentrated acids required for 1000 kg of desired mixed acid.

## OR

Q. 3 (a) Define (a) Adiabatic saturation temperature (b) Wet bulb Temperature (c) Molal humidity
(b) Define NCV and GCV.
(c) A Feed containing $50 \%$ benzene and $50 \%$ toluene is fed to a distillation column at the rate of $5000 \mathrm{~kg} / \mathrm{h}$. The top product contains $95 \%$ benzene and bottom product contains $92 \%$ toluene by weight. Calculate (a) the mass flow rates of top and bottom products and (b) the percent recovery of benzene.
Q. 4 (a) 98 grams of sulphuric acid are dissolved in water to prepare one litre of03solution. Find normality and molarity of solution.
(b) Write down statement of Amagat's law with mathematical expression. ..... 04
(c) A mixture of acetone vapour and nitrogen contains $14.8 \%$ acetone by ..... 07 volume. Calculate the following at 293 K and a pressure of 99.33 kPa .
(a) Partial pressure of acetone.
(b) Moles of acetone per mole of nitrogen.
(c) Relative saturation of mixture at 293 K .
(d) Percentage saturation of mixture at 293 K .
Data: Vapour pressure of acetone at $293 \mathrm{~K}=24.638 \mathrm{kPa}$

## OR

Q. 4 (a) Write in brief about selectivity.
(b) Brief about raoult's law and henry's law for gas-liquid system.
(c) A mixture of benzene vapour and nitrogen gas at 297 K and 100 kPa has a relative humidity of $60 \%$. It is desired to recover $80 \%$ of benzene by cooling a mixture to 283 K and compressing to a suitable pressure. Find out the pressure required for above duty.
Data: Vapour pressure of benzene at $297 \mathrm{~K}=12.2 \mathrm{kPa}$
Q. 5 (a) 2000 kg of wet solids by weight are fed to a tray dryer where it is dried by hot air. The product finally obtained is found to contain $1 \%$ moisture by weight, calculate:
(a) The kg of water removed from solids,
(b) The kg of product obtained.
 (volume) acetone by scrubbing with water. Assuming that air is insoluble in water, determine the percent of acetone in the entering gas that is absorbed if the gas leaving the scrubber analyzes 5\% acetone.
(c) Explain orsat analysis with diagram.
Q. 5 (a) Draw neat sketch of Recycle, bypass and purge operations with explanation.
(b) A continuous distillation column is used to regenerate solvent for use in a solvent extraction unit. The column treats $200 \mathrm{kmol} / \mathrm{hr}$ of a feed containing $10 \%$ mole ethyl alcohol and the rest is water. The overhead product is $89 \%$ mole alcohol and the bottom product is $0.3 \%$ mole alcohol. The overhead product is sent to the extraction unit and the bottom is wasted. What is the daily requirement of make-up alcohol in the solvent extraction unit?
(c) A purified brine at the rate of $50 \mathrm{~kg} / \mathrm{h}$ is sent to an electrolytic cell for producing chlorine:
$2 \mathrm{NaCl}+2 \mathrm{H}_{2} \mathrm{O} \longrightarrow 2 \mathrm{NaOH}+\mathrm{Cl}_{2}+\mathrm{H}_{2}$
Only $50 \%$ of NaCl in the charge is electrolyzed. The gases leaving the cell carry with them water vapour in the ratio $0.03 \mathrm{~mol} / \mathrm{mol}$ gas formed. The solution leaving the cell contains $10 \% \mathrm{NaOH}$ which is concentrated to $50 \%$ NaOH in evaporators. The NaCl present in the solution fed to the evaporator is crystallized and removed so that the concentrate leaving the evaporators contain only $1.5 \% \mathrm{NaCl}$. Calculate the following :
(a) The rate of production of $50 \% \mathrm{NaOH}$ in $\mathrm{kg} / \mathrm{h}$
(b) The rate of production of chlorine and hydrogen gas
(c) The rate at which NaCl is crystallized in $\mathrm{kg} / \mathrm{h}$.

