03



Q.1

Q.2

Sea	nt No.: Enrolment No						
Su Tin Inst 1. A 2. N	GUJARAT TECHNOLOGICAL UNIVERSITY BE - SEMESTER- VI (New) EXAMINATION - WINTER 2019 bject Code: 2161403 Date: 06/12/2019 bject Name: Food Engineering Operations - II me: 02:30 PM TO 05:00 PM Total Marks: 70 tructions: Attempt all questions. Make suitable assumptions wherever necessary. Figures to the right indicate full marks.						
(a)	How does homogenization of milk increases its stability? What are the effects of homogenization on properties of milk?	03					
(b)	Differentiate between pasteurization and Sterilization. List out the advantages of Heat Exchangers over in-bottle processing in pasteurization.	04					
(c)	Write short notes on: Crystal growth and Circulating magma vacuum crystallizer						
(a) (b)	 The F value at 121.1 °C equivalent to 99.999% inactivation of a strain of <i>C. botulinum</i> is 1.5 minutes. (i) Calculate the D₀ value of this organism. (ii) Calculate F₀ based on the 12D concept using the D₀ value of <i>C. botulinum</i> and a most likely spore load in the product of 100 What are the main components of a homogenizer? Calculate the power (in kW) required to start up a centrifugal separator with the following data: 	03					
	Density of bowl = 7850 kg/m^3						
	Speed of rotation = 6000 rpm Outer radius of disc = 0.25 m and inner radius of disc = 0.225 m Length where the mass is concentrated = 0.325 m Time to reach the running speed = 3 minutes						
(c)	Describe the function of a regenerator in a HTST pasteurizer. Draw the line diagram of a HTST pasteurizer labeling each component.	07					
	OR						
(c)	What do you mean by Fouling of heat exchangers? Briefly explain the types of fouling deposits in heat exchanger used in milk pasteurizer and their effect on performance. How descaling of	07					

heat exchanger is done?

Q.3 (a) Explain flash distillation with figure.



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	(b)	What are the advantages a			04						
	(c)	What do you mean by bact of milk in a centrifugal dis	_							•	07
					C)R					
Q.3	(a)	Define D- value, Z- Value	and r	epresei	nt them	graphica	ally.				03
	(b)	Briefly explain the influence of freezing process on the thermal properties of the food products.									
	(c)	List out different types of f system. Mention two most		_	•			ly the fluidized bed IQF freezing ersion freezing system.			
Q.4	(a)	Differentiate between dist	entiate between distillation and liquid-liquid extraction.								
	(b)	Explain mechanism of crystallization in detail.									04
	(c)	Derive an equation of rectifying section operating line for fractional distillation column.									07
					C)R					
Q.4	(a)	What is the principle of cl	arifyir	ng filte	rs?						03
	(b)	Explain in detail about cal	ke filte	ers.							04
	(c)										07
Q.5	(a)	equilateral triangular diagram for Single-stage liquid-liquid extraction process. Explain significance of relative volatility in distillation. 03									
Q.S	` ,										
	(b)	Describe in brief about batch sedimentation and draw the neat diagram indicating the same. 0									04
	(c)	An equimolar mixture of benzene and toluene is subjected to flash distillation at a pressure of 07									
		1 bar in the separator. Det		_	-	•			,	•	
		vapour leaving the separa				25% va	porized	. Equili	brium d	ata for benzene-	
		toluene system at 1 bar is	given	ın Tab	le:						
		Temperature °C	80.1	85	90	95	100	105	110.6		
		Mole fraction Benzene	1	0.78	0.581	0.411	0.258	0.13	0		
		in liquid	1	0.0	0.777	0.622	0.456	0.261	0		
		Mole fraction Benzene	1	0.9	0.777	0.032	0.456	0.261	0		

OR

Q.5 (a) Write a short note on filter aids.

in vapor

(b) A solution containing 10g/lit of a valuable protein and 1g/lit of a protein impurity is extracted in a stirred vessel using an organic solvent. Distribution co-efficient K=8 for the valuable proteins and 0.5 for the impurity. The initial volume is 500 lit and 400 lit of solvent are used





for the extraction. What are the final concentration in the two phases and what fraction of each proteins is recovered in the solvent phase?

(c) A continuous fractionating column is to be designed for separating 10,000 kg per hour of a liquid mixture containing 40 mole percent methanol and 60 mole percent water into an overhead product containing 97 mole percent methanol and a bottom product having 98 mole percent water. A mole reflux ratio of 3 is used. Calculate (i) moles of overhead product obtained per hour and (ii) number of ideal plates and location of the feed plate if the feed is at its bubble point.

Equilibrium data:

x	0.1	0.2	0.3	0.4	0.5	0.6	0.7	0.8	0.9
у	0.417	0.579	0.669	0.729	0.78	0.825	0.871	0.915	0.959

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