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GUJARAT TECHNOLOGICAL UNIVERSITY

BE - SEMESTER- VII (New) EXAMINATION - WINTER 2019 Date: 03/12/2019

Subject Code: 2171306

Subject Name: Wastewater Engineering

Time: 10:30 AM TO 01:30 PM

Instructions:

- 1. Attempt all questions.
- 2. Make suitable assumptions wherever necessary.
- 3. Figures to the right indicate full marks.
- Write down operational problems with its solution occurred in aerated grit 03 **Q.1** (a) chamber.
 - (b) A wastewater flow of 0.60 m³/min containing 150 mg/L of oil and grease is to be 04 reduced to a concentration of 25 mg/L. Assuming the following data, design a dissolved air flotation system.

Surface loading rate (SLR) = 130 L/m^2 -min; Wastewater temperature = 35° C; Air solubility at 35°C (S_a) = 17.15 ml/L; A/S = 0.025 (mL/mg); Fraction of air saturation (f) = 0.80 and Recycle system pressure = 500 kPa.

Determine the size, dimensions and HRT of a UASB reactor which will be used (c) for the treatment of an industrial effluent. The wastewater is mainly soluble, containing carbohydrate compounds and a granular sludge is expected. Suppose 90% soluble COD removal, 50% of the influent pCOD degraded and 90% of influent sulfate is reduced biologically. Methane production at $35^{\circ}C = 0.40$ L CH₄/g COD; Reactor volume effectiveness factor = 85%, density of methane at $30^{\circ}\text{C} = 0.6451 \text{ g/L}$ and height for gas collection = 2.5 m. Also determine total gas production (assuming 65% methane), energy available from methane and alkalinity requirements.

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Item	Value
Flow Rate	1000 m ³ /day
COD	2300 mg/L
sCOD	2000 mg/L
Alkalinity	500 mg/L as CaCo ₃
SO_4	200 mg/L
Temperature	30°C

- Q.2 (a) Differentiate between domestic wastewater and industrial wastewater.
 - Design a cylindrical flash mixing tank by determining the tank dimensions and 04 **(b)** required input power using following data: Design flow rate = $11.5 \times 10^3 \text{ m}^3/\text{d}$, Rapid Mix time= 5 s, Rapid mix G =600 s⁻¹ and $\mu = 1.5195 \times 10^{-3} \text{ N/m}^2$.s..
 - Design a grit chamber having a rectangular cross-section and a proportional weir (c) as the velocity control device, with the following supplied data: Maximum flow = 12 MLD; Maximum temperature = 26° C; Minimum temperature = 15° C; Specific gravity of grit particles = 2.65 and Diameter of smallest grit particles to be removed = 0.02 cm.

OR

- (c) Assuming suitable design criteria, compute the dimensions of a rectangular 07 settling tank to remove suspended flocculent particles from the average wastewater flow of 15000 m³/d. A column test indicates that an overflow rate of 40 m/d will produce satisfactory removal of suspended floc at 3.5 m depth.
- Q.3 (a) Write down operational problems of UASB.

MARKS



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- FirstRanker.com FirstRanker.com $BOD_5 = 175 \text{ mg/L} \&$ to be operated at 25°C. The depth of modular plastic media to be used is 6.0 m & recirculation ratio will be 2:1. The treatability constant determined at 20° C = 0.06 min⁻¹ & desirable concentration of effluent is 20 mg/L. Assuming suitable design criteria, design a trickling filter system to treat an 07 (c) average domestic wastewater flow of 10 MLD having influent BOD₅ equal to 250 mg/L. The desired effluent BOD₅ is 25 mg/L or less. OR (a) Write the Eckenfelder equations (with & without recirculation) for Bio tower Q.3 03 design. (b) Enlist and Explain the operational problems of chemical unit operations. 04 Estimate the size of digester required to treat the sludge from a primary treatment 07 (c) plant designed to treat 38000 m³/d of wastewater. Check the volumetric loading, estimate percent stabilization and the amount of gas produced. For wastewater to be treated, it has been found that the quantity of dry volatile solids and biodegradable COD removed is 0.15 Kg/m^3 and 0.14 Kg/m^3 , respectively. Assume that the sludge contains about 95% moisture and has a specific gravity of 1.02. Assume hydraulic regime of the reactor is complete mix. (SRT =10 days @ 35° C; Efficiency of waste utilization =0.70; Y =0.08 Kg VSS/Kg bCOD utilized; $k_d =$ $0.03 d^{-1}$ and digester gas is 65% methane) (a) Explain the factors responsible for bulking of sludge. 03 0.4 An activated sludge plant is to be designed for 10 MLD domestic wastewater flow 04 **(b)** to operate at 10 days MCRT and 6 hours of HRT. Assuming BOD₅ 20°C as 175 mg/L in influent to the aeration tank, sludge wasting flow equal to 70 m³/d and return sludge concentration equal to 8000 mg/L, determine the concentration of MLVSS to be maintained in the aeration tank to achieve effluent BOD₅ of 30 mg/L. Also determine the recirculation ratio at which plant should be operated. Assume the kinetic coefficients $K_d = 0.06 d^{-1}$ and Y = 0.6.
 - (c) Explain the phases of SBR operational cycle with neat sketch.

OR

- 0.4 (a) Write a short note on extended aeration. 03 (b) Explain the working mechanism of Rotating Biological Contractor with neat 04 sketch.
 - Design a rotating biological contactor to treat 10 MLD flow of municipal 07 (c) wastewater having BOD₅ concentration of 250 mg/L. The primary treatment removes 30 % raw BOD₅ and desired effluent BOD₅ is 250 mg/L. Assume 0.05 m^3/m^2 -d hydraulic loading and other suitable data if needed.
- **Q.5** Enlist and explain the types of filter presses. **(a)**
 - Explain various methods of dewatering of sludge. **(b)**
 - Design sludge drying beds to dewater the digested sludge produced from 07 (c) wastewater treatment plant based on the activated sludge process designed for 50000 population. Assume other suitable data.

OR

- Define the following terms: (i) Sludge volume index, (ii) Mean cell residence time 03 0.5 (a) and (iii) Mixed liquor suspended solids
 - (b) Explain various methods of thickening of sludge. 04
 - (c) Write a short note on "Natural evaporation "as a treatment of wastewater. 07

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04