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## **GUJARAT TECHNOLOGICAL UNIVERSITY** BE - SEMESTER-V (NEW) EXAMINATION – WINTER 2018

Subject Code:2150503

Date:16/11/2018

Subject Name: Chemical Engineering Thermodynamics-II

Time: 10:30 AM TO 01:00 PM

**Total Marks: 70** 

Instructions:

- 1. Attempt all questions.
- 2. Make suitable assumptions wherever necessary.
- 3. Figures to the right indicate full marks.
- Q.1 (a) For binary azeotropic mixture deviating positively from ideality, draw vapor-liquid 03 equilibrium (VLE) diagrams.
  - (b) Describe phase rule and Duhem's theorem for non-reacting system. 04
  - (c) Define Lewis/Randall Rule. Derive Raoult's law. What are the limitations of 07 Raoult's law?
- **Q.2** (a) With neat diagram describe the effect of increasing pressure on binary T-x<sub>1</sub>,y<sub>1</sub> vapor- 03 liquid equilibrium diagram.
  - (b) Describe the phenomena of retrograde condensation.
  - (c) Assuming validity of Raoult's law, draw P-x<sub>1</sub>,y<sub>1</sub> diagram for binary mixture at 75 07 <sup>0</sup>C. Clearly show vapor region, liquid region, bubble point and dew point curves. Data given:

At 75  ${}^{0}$ C, P<sub>1</sub><sup>sat</sup>=83.21 kPa and P<sub>2</sub><sup>sat</sup>=41.98 kPa

(c) System acetone(1)/acetonitrile(2)/nitromethane(3) at 353.15 K has the overall **07** composition  $z_1 = 0.45$ ,  $z_2 = 0.35$  and  $z_3 = 0.20$ . Assuming that the Raoult's law is appropriate to this system, determine equilibrium pressure and vapor-liquid composition to carry out 40% vaporization. Date Given: The vapor pressures of the pure species at the 353.15 K are:

 $P_1^{sat} = 195.75 \text{ kPa}, P_2^{sat} = 97.84 \text{ kPa} \text{ and } P_3^{sat} = 50.32 \text{ kPa}$ 

- Q.3 (a) Define: (1) thermodynamic equilibrium, (2) chemical potential, and (3) fugacity 03 coefficient for pure species i.
  - (b) Describe graphical interpretation of following two equations relating partial molar 04 properties with solution properties.

$$\overline{\mathbf{M}}_1 = \mathbf{M} + \mathbf{x}_2 \frac{\mathrm{d}\mathbf{M}}{\mathrm{d}\mathbf{x}_1}$$
 and  $\overline{\mathbf{M}}_2 = \mathbf{M} - \mathbf{x}_1 \frac{\mathrm{d}\mathbf{M}}{\mathrm{d}\mathbf{x}_1}$ 

(c) Will it be possible to prepare  $0.1 \text{ m}^3$  of ethanol-water solution by mixing  $0.03 \text{ m}^3$  **07** ethanol with  $0.07 \text{ m}^3$  pure water? If not possible, what volume should have been mixed in order to prepare a mixture of the same strength and of required volume? Density of ethanol and water are 789 and 997 kg/m<sup>3</sup>, respectively. The partial molar volumes of ethanol and water at the desired compositions are: Ethanol = 53.6 x  $10^{-6} \text{ m}^3/\text{mol}$ ; water =  $18 \times 10^{-6} \text{ m}^3/\text{mol}$ .

04

Q.3<sup>st</sup>(a) <sup>k</sup>For<sup>s</sup>ideal gases, prove that the mastic angler comme is identical with through epecies 03 volume at the mixture T and P.

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 $\overline{V}_{i}^{ig} = V_{i}^{ig}$ 

(b) For binary mixture derive following equations to calculate fugacity coefficient from 04 virial equation of state.

$$\ln\hat{\varphi}_1 = \frac{P}{RT} \left( B_{11} + y_2^2 \delta_{12} \right)$$

- (c) Derive an expression for the fugacity coefficient of a gas obeying the equation of 07 state P(V-b)=R T and estimate the fugacity of ammonia at 10 bar and 298 K, given that  $b = 3.707 \times 10^{-5} \text{ m}^3/\text{mol}$ .
- Q.4 (a) Liquids A and B form an azeotrope containing 46.1 mole percent A at 101.3 kPa and 03 345 K. At 345 K, the vapor pressure of A is 84.8 kPa and that of B is 78.2 kPa. Calculate the van Laar constants.

(c) Describe Wilson and NRTL equations with their applications and limitations. 07

## OR

03

03

07

**Q.4** (a) Describe Poynting correction.

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- (b) Discuss the effect of temperature, pressure and liquid phase composition on relative 04 volatility of binary mixture following modified Raoult's law.
- (c) The activity coefficients in a binary system are given by  $\ln\gamma_1 = Ax_2^2$  and  $\ln\gamma_2 = Ax_1^2$ . 07 Show that if the system forms an azoetrope, then azeotropic composition is given by

$$\mathbf{x}_{1}^{\mathrm{az}} = \frac{1}{2} \left[ 1 - \frac{1}{A} \ln \left( \frac{\mathbf{P}_{2}^{\mathrm{sat}}}{\mathbf{P}_{1}^{\mathrm{sat}}} \right) \right]$$

- **Q.5** (a) Describe effect of temperature on reaction equilibrium constant.
  - (b) Develop expressions for the mole fractions of reacting species as functions of the 04 reaction coordinate for:
    - (1) A system initially containing 2 mol  $NH_3$  and 5 mol  $O_2$  and undergoes the reaction:

$$4NH_3(g) + 5O_2(g) \rightarrow 4NO(g) + 6H_2O(g)$$

(2) A system initially containing 3 mol  $H_2S$  and 5 mol  $O_2$  and undergoing the reaction:

$$2H_2S(g) + 3O_2(g) \rightarrow 2H_2O(g) + 2SO_2(g)$$

(c) Explain block diagram for dew point pressure calculation.

## OR

- Q.5 (a) If  $G^E/RT = A x_1 x_2$  for a liquid phase, show by stability analysis that LLE is predicted 03 for  $A \ge 2$ .
  - (b) Briefly describe constant pressure liquid/liquid solubility diagrams. 04
  - (c) Explain the method of Lagrange's undetermined multipliers for gas phase reaction 07 to minimize total Gibbs free energy.

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