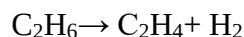


GUJARAT TECHNOLOGICAL UNIVERSITY**BE - SEMESTER-VI (NEW) EXAMINATION – WINTER 2018****Subject Code:2160506****Date:07/12/2018****Subject Name:Chemical Reaction Engineering - I****Time: 02:30 PM TO 05:00 PM****Total Marks: 70****Instructions:**

1. Attempt all questions.
2. Make suitable assumptions wherever necessary.
3. Figures to the right indicate full marks.

- Q.1**
- (a) Classify reactions giving example of each **03**
- (b) Differentiate elementary and non elementary reactions. **04**
- (c) List various theories of temperature dependency on rate of reaction and discuss any one in detail. **07**
- Q.2**
- (a) Write a short note on 'Variable volume batch reactor' **03**
- (b) The rate constant k at 27°C is $1.3 \times 10^{-3} \text{sec}^{-1}$ and its frequency factor is $2.785 \times 10^{-6} \text{sec}^{-1}$. Determine its Entropy of activation and Enthalpy of activation. **04**
- (c) Derive integrated rate expression for a liquid phase reaction **07**
 $2A \rightarrow \text{Products.}$
- OR**
- (c) At certain temperature, the half-life period and initial concentration for a reaction are, **07**
 $t_{1/2} = 420 \text{ sec}; C_{A0} = 0.405 \text{ mole/lit}$
 $t_{1/2} = 275 \text{ sec}; C_{A0} = 0.640 \text{ mole/lit}$
Calculate the order of reaction and rate constant of the reaction.
- Q.3**
- (a) Define space time and space velocity. **03**
- (b) Derive performance equation for a ideal batch reactor **04**
- (c) The reaction $A \rightarrow B$, $r = k C_{A0}^2$, occurs in CSTR with 90% Conversion, if $k = 0.5 \text{ liter/mole min}$, $C_{A0} = 2 \text{ mole/liter}$ and $v = 4 \text{ liter/min}$, what residence time and reactor volume will be required? **07**
- OR**
- Q.3**
- (a) Explain the method for searching the mechanism of chemical reaction. **03**
- (b) Compare and contrast Integral method of analysis with differential method of analysis of kinetic data. **04**
- (c) In a batch reactor, assuming first order kinetics, the conversion of a liquid reactant A is 70% in 13 min. Find the space time required to effect this conversion in a plug flow reactor and a mixed flow reactor. **07**
- Q.4**
- (a) Discuss equal sized mixed flow reactors in series **03**
- (b) Derive performance equation for a CSTR. **04**

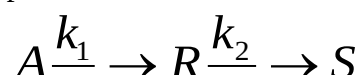
- (c) The thermal cracking of ethane is carried out in a tubular reactor for large scale production of ethylene. The reaction is 07



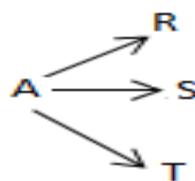
The ethane fed at the rate of 10 tons/hr, is diluted with steam (0.5 mole of steam: 1 mole of Ethane) before entering the reactor to reduce amount of undesired products. The reaction is maintained at 900 °C and 1.4 atm total pressures. Reaction is first order irreversible and rate constant is 12.8 sec⁻¹ at 900°C. Calculate the volume of reactor required for 60% conversion of ethane per pass.

OR

- Q.4** (a) Show how fractional conversion X , is related to temperature for any exothermic reaction being carried out in an adiabatic batch reactor. 03
(b) Write a short note on Recycle reactor. 04
(c) Derive the equation in terms of concentration for irreversible reactions in series for uni-molecular type first-order reaction such as 07



- Q.5** (a) Discuss the effect of pressure on equilibrium conversion as predicted by thermodynamics keeping temperature fixed 03
(b) Discuss the method of maximization of rectangles applied to find the optimum intermediate conversion and optimum sizes of two mixed reactors in series 04
(c) For the parallel decomposition of A where R is desired and $C_{A0} = 1$ 07



What is the maximum C_R , we may expect in an isothermal operation in Batch Reactor, where the value of $r_R = 1$, $r_S = 2C_A$, $r_T = C_A^2$

OR

- Q.5** (a) Discuss the effect of inert on equilibrium conversion as predicted by thermodynamics keeping temperature fixed 03
(b) Explain optimum temperature progression in brief. 04
(c) Describe quantitative discussion about product distribution for reactions in parallel. 07
