

Code No: R05310803

**R05****Set No. 2**

**III B.Tech I Semester Examinations, November 2010**  
**CHEMICAL ENGINEERING THERMODYNAMICS-II**

**Chemical Engineering**

Time: 3 hours

Max Marks: 80

**Answer any FIVE Questions**  
**All Questions carry equal marks**

\*\*\*\*\*

- Derive Clapeyron equation
  - Calculate the amount of heat given off when 1 m<sup>3</sup> of air ( at S.T.P) cools from 500 °C to -100 °C at constant pressure of 1 atmosphere. Heat capacity constants:

$$C_p = a + bT + cT^2 \text{ (cal/ mol. K).} \quad [6+10]$$

	a	B * 10 <sup>3</sup>	C * 10 <sup>6</sup>
N <sub>2</sub>	6.457	1.389	-0.069
O <sub>2</sub>	6.117	3.167	-1.005

- In a laboratory investigation, acetylene is catalytically hydrogenated to ethylene at 1,120°C And 1 bar. If the feed is an equimolar mixture of acetylene and hydrogen, what is the composition of the product stream at equilibrium? The reactions are  
 $C_2H_2 \rightarrow 2C + H_2$   
 $2C + 2H_2 \rightarrow C_2H_4$   
 $K_1 = 4 \times 10^5, \quad K_2 = 2.5 \times 10^{-6}.$  [16]

- Carbon monoxide at 100 °C is burned under atmospheric pressure with dry air at 400 °C is 30% excess of that theoretically required. The products of combustion leave the reaction chamber at 900 °C. Calculate the heat evolved in the reaction chamber in k cal/ kg mole of CO burned, assuming complete combustion:

$$\Delta H_{25} = -67,636 \text{ k cal}$$

Mean molal heat capacities in the temp. range involved are

$$CO = 7.017 \text{ gm cal/ gm mole } ^\circ K$$

$$\text{Air} = 7.225 \text{ gm cal/ gm mole } ^\circ K$$

$$CO_2 = 11.92 \text{ gm cal/ gm mole } ^\circ K$$

$$O_2 = 7.941 \text{ gm cal/ gm mole } ^\circ K$$

$$N_2 = 7.507 \text{ gm cal/ gm mole } ^\circ K.$$
 [16]

- Flash calculations are simpler for binary system than for multicomponent case, show that, for a binary system in VLE,  $x_1 = \frac{1-k_2}{k_1-k_2}, y = \frac{k_1(1-k_2)}{k_1-k_2}$   

$$\vartheta = \frac{Z_1(k_1-k_2)-(1-k_2)}{(k_1-1)(1-k_2)}.$$
 [16]

- Discuss about liquid-liquid Equilibrium (LLE). Draw liquid-liquid solubility diagram with proper labeling. [16]

- Discuss about Bubble point and dew point using P-xy diagram.

- Discuss about flash calculations. [8+8]

Code No: R05310803

**R05****Set No. 2**

7. The enthalpy of a binary liquid system of species 1 and 2 at fixed T and P is represented by the equation  $H = 400x_1 + 600x_2 + x_1 x_2 (20x_2 + 40x_1)$  Where H is in J mol<sup>-1</sup>. Determine the expression for partial property for enthalpy for component 1 and 2 as function of  $x_1$ , numerical values for the pure species, and also numerical values for the partial enthalpies at infinite dilution. [16]
8. Plot equilibrium curve (p-x-y) for ethyl alcohol- water system using Vanlaar method. The data needed to solve the problem by Vanlaar method is as follow:- Ethanol-water system forms an azetrope at 78.15 °C, 1 atm and corresponding ethanol composition is 89.43 mole% Vapour pressure of water and ethanol at 78.15 °C are 329 mm Hg and 755 mm Hg respectively. [16]

\*\*\*\*\*

FIRSTRANKER

Code No: R05310803

**R05****Set No. 4**

**III B.Tech I Semester Examinations, November 2010**  
**CHEMICAL ENGINEERING THERMODYNAMICS-II**

**Chemical Engineering**

Time: 3 hours

Max Marks: 80

**Answer any FIVE Questions**  
**All Questions carry equal marks**

\*\*\*\*\*

- In a laboratory investigation, acetylene is catalytically hydrogenated to ethylene at 1,120°C And 1 bar. If the feed is an equimolar mixture of acetylene and hydrogen, what is the composition of the product stream at equilibrium? The reactions are  
 $C_2H_2 \rightarrow 2C + H_2$        $K_1 = 4 \times 10^5$ ,     $K_2 = 2.5 \times 10^{-6}$ .  
 $2C + 2H_2 \rightarrow C_2H_4$  [16]
  - Plot equilibrium curve (p-x-y) for ethyl alcohol- water system using Vanlaar method. The data needed to solve the problem by Vanlaar method is as follow:- Ethanol-water system forms an azeotrope at 78.15 °C, 1 atm and corresponding ethanol composition is 89.43 mole% Vapour pressure of water and ethanol at 78.15 °C are 329 mm Hg and 755 mm Hg respectively. [16]
  - (a) Derive Clapeyron equation  
 (b) Calculate the amount of heat given off when 1 m<sup>3</sup> of air ( at S.T.P) cools from 500 °C to -100 °C at constant pressure of 1 atmosphere. Heat capacity constants:  
 $C_p = a + bT + cT^2$  (cal/ mol. K). [6+10]
- |                | a     | B * 10 <sup>3</sup> | C * 10 <sup>6</sup> |
|----------------|-------|---------------------|---------------------|
| N <sub>2</sub> | 6.457 | 1.389               | -0.069              |
| O <sub>2</sub> | 6.117 | 3.167               | -1.005              |
- The enthalpy of a binary liquid system of species 1 and 2 at fixed T and P is represented by the equation  $H = 400x_1 + 600x_2 + x_1 x_2 (20 x_2 + 40x_1)$  Where H is in J mol<sup>-1</sup>. Determine the expression for partial property for enthalpy for component 1 and 2 as function of x<sub>1</sub>, numerical values for the pure species, and also numerical values for the partial enthalpies at infinite dilution. [16]
  - (a) Discuss about Bubble point and dew point using P-xy diagram.  
 (b) Discuss about flash calculations. [8+8]
  - Discuss about liquid-liquid Equilibrium (LLE). Draw liquid-liquid solubility diagram with proper labeling. [16]
  - Carbon monoxide at 100 °C is burned under atmospheric pressure with dry air at 400 °C is 30% excess of that theoretically required. The products of combustion leave the reaction chamber at 900 °C. Calculate the heat evolved in the reaction chamber in k cal/ kg mole of CO burned, assuming complete combustion:  
 $\Delta H_{25} = -67,636$  k cal  
 Mean molal heat capacities in the temp. range involved are

Code No: R05310803

**R05****Set No. 4**

$$\text{CO} = 7.017 \text{ gm cal/ gm mole } ^\circ\text{K}$$

$$\text{Air} = 7.225 \text{ gm cal/ gm mole } ^\circ\text{K}$$

$$\text{CO}_2 = 11.92 \text{ gm cal/ gm mole } ^\circ\text{K}$$

$$\text{O}_2 = 7.941 \text{ gm cal/ gm mole } ^\circ\text{K}$$

$$\text{N}_2 = 7.507 \text{ gm cal/ gm mole } ^\circ\text{K}.$$

[16]

8. Flash calculations are simpler for binary system than for multicomponent case, show that, for a binary system in VLE,  $x_1 = \frac{1-k_2}{k_1-k_2}$ ,  $y = \frac{k_1(1-k_2)}{k_1-k_2}$

$$\vartheta = \frac{Z_1(k_1-k_2)-(1-k_2)}{(k_1-1)(1-k_2)}.$$

[16]

\*\*\*\*\*

FIRSTRANKER

Code No: R05310803

**R05****Set No. 1**

**III B.Tech I Semester Examinations, November 2010**  
**CHEMICAL ENGINEERING THERMODYNAMICS-II**

**Chemical Engineering**

Time: 3 hours

Max Marks: 80

**Answer any FIVE Questions**  
**All Questions carry equal marks**

\*\*\*\*\*

- In a laboratory investigation, acetylene is catalytically hydrogenated to ethylene at 1,120°C And 1 bar. If the feed is an equimolar mixture of acetylene and hydrogen, what is the composition of the product stream at equilibrium? The reactions are  

$$C_2H_2 \rightarrow 2C + H_2 \quad K_1 = 4 \times 10^5, \quad K_2 = 2.5 \times 10^{-6}$$

$$2C + 2H_2 \rightarrow C_2H_4$$

[16]
- Flash calculations are simpler for binary system than for multicomponent case, show that, for a binary system in VLE,  $x_1 = \frac{1-k_2}{k_1-k_2}$ ,  $y = \frac{k_1(1-k_2)}{k_1-k_2}$   

$$\vartheta = \frac{Z_1(k_1-k_2)-(1-k_2)}{(k_1-1)(1-k_2)}$$

[16]
- Derive Clapeyron equation
  - Calculate the amount of heat given off when 1 m<sup>3</sup> of air ( at S.T.P) cools from 500 °C to -100 °C at constant pressure of 1 atmosphere. Heat capacity constants:  

$$C_p = a + bT + cT^2 \text{ (cal/ mol. K).}$$

[6+10]

	a	B * 10 <sup>3</sup>	C * 10 <sup>6</sup>
N <sub>2</sub>	6.457	1.389	-0.069
O <sub>2</sub>	6.117	3.167	-1.005
- Discuss about liquid-liquid Equilibrium (LLE). Draw liquid-liquid solubility diagram with proper labeling.

[16]
- Carbon monoxide at 100 °C is burned under atmospheric pressure with dry air at 400 °C is 30% excess of that theoretically required. The products of combustion leave the reaction chamber at 900 °C. Calculate the heat evolved in the reaction chamber in k cal/ kg mole of CO burned, assuming complete combustion:  
 $\Delta H_{25} = -67,636 \text{ k cal}$   
Mean molal heat capacities in the temp. range involved are  
CO = 7.017 gm cal/ gm mole °K  
Air = 7.225 gm cal/ gm mole °K  
CO<sub>2</sub> = 11.92 gm cal/ gm mole °K  
O<sub>2</sub> = 7.941 gm cal/ gm mole °K  
N<sub>2</sub> = 7.507 gm cal/ gm mole °K.

[16]
- The enthalpy of a binary liquid system of species 1 and 2 at fixed T and P is represented by the equation  $H = 400x_1 + 600x_2 + x_1 x_2 (20 x_2 + 40x_1)$  Where H is in J mol<sup>-1</sup>. Determine the expression for partial property for enthalpy for component 1 and 2 as function of x<sub>1</sub>, numerical values for the pure species, and also numerical values for the partial enthalpies at infinite dilution.

[16]

Code No: R05310803

**R05****Set No. 1**

7. (a) Discuss about Bubble point and dew point using P-xy diagram.  
(b) Discuss about flash calculations. [8+8]
8. Plot equilibrium curve (p-x-y) for ethyl alcohol- water system using Vanlaar method. The data needed to solve the problem by Vanlaar method is as follow:- Ethanol-water system forms an azeotrope at 78.15 °C, 1 atm and corresponding ethanol composition is 89.43 mole% Vapour pressure of water and ethanol at 78.15 °C are 329 mm Hg and 755 mm Hg respectively. [16]

\*\*\*\*\*

FIRSTRANKER

Code No: R05310803

**R05****Set No. 3**

**III B.Tech I Semester Examinations, November 2010**  
**CHEMICAL ENGINEERING THERMODYNAMICS-II**

**Chemical Engineering**

Time: 3 hours

Max Marks: 80

**Answer any FIVE Questions**  
**All Questions carry equal marks**

\*\*\*\*\*

- In a laboratory investigation, acetylene is catalytically hydrogenated to ethylene at 1,120°C and 1 bar. If the feed is an equimolar mixture of acetylene and hydrogen, what is the composition of the product stream at equilibrium? The reactions are  
 $C_2H_2 \rightarrow 2C + H_2$        $K_1 = 4 \times 10^5$ ,     $K_2 = 2.5 \times 10^{-6}$ .  
 $2C + 2H_2 \rightarrow C_2H_4$  [16]
  - (a) Discuss about Bubble point and dew point using P-xy diagram.  
 (b) Discuss about flash calculations. [8+8]
  - (a) Derive Clapeyron equation  
 (b) Calculate the amount of heat given off when 1 m<sup>3</sup> of air (at S.T.P) cools from 500 °C to -100 °C at constant pressure of 1 atmosphere. Heat capacity constants:  
 $C_p = a + bT + cT^2$  (cal/ mol. K). [6+10]
- |                | a     | B * 10 <sup>3</sup> | C * 10 <sup>6</sup> |
|----------------|-------|---------------------|---------------------|
| N <sub>2</sub> | 6.457 | 1.389               | -0.069              |
| O <sub>2</sub> | 6.117 | 3.167               | -1.005              |
- Flash calculations are simpler for binary system than for multicomponent case, show that, for a binary system in VLE,  $x_1 = \frac{1-k_2}{k_1-k_2}$ ,  $y = \frac{k_1(1-k_2)}{k_1-k_2}$   
 $\vartheta = \frac{Z_1(k_1-k_2)-(1-k_2)}{(k_1-1)(1-k_2)}$ . [16]
  - Discuss about liquid-liquid Equilibrium (LLE). Draw liquid-liquid solubility diagram with proper labeling. [16]
  - Plot equilibrium curve (p-x-y) for ethyl alcohol- water system using Vanlaar method. The data needed to solve the problem by Vanlaar method is as follow:- Ethanol-water system forms an azeotrope at 78.15 °C, 1 atm and corresponding ethanol composition is 89.43 mole% Vapour pressure of water and ethanol at 78.15 °C are 329 mm Hg and 755 mm Hg respectively. [16]
  - The enthalpy of a binary liquid system of species 1 and 2 at fixed T and P is represented by the equation  $H = 400x_1 + 600x_2 + x_1 x_2 (20 x_2 + 40 x_1)$  Where H is in J mol<sup>-1</sup>. Determine the expression for partial property for enthalpy for component 1 and 2 as function of x<sub>1</sub>, numerical values for the pure species, and also numerical values for the partial enthalpies at infinite dilution. [16]

Code No: R05310803

**R05****Set No. 3**

8. Carbon monoxide at 100 °C is burned under atmospheric pressure with dry air at 400 °C is 30% excess of that theoretically required. The products of combustion leave the reaction chamber at 900 °C. Calculate the heat evolved in the reaction chamber in k cal/ kg mole of CO burned, assuming complete combustion:

$$\Delta H_{25} = -67,636 \text{ k cal}$$

Mean molal heat capacities in the temp. range involved are

$$\text{CO} = 7.017 \text{ gm cal/ gm mole } ^\circ\text{K}$$

$$\text{Air} = 7.225 \text{ gm cal/ gm mole } ^\circ\text{K}$$

$$\text{CO}_2 = 11.92 \text{ gm cal/ gm mole } ^\circ\text{K}$$

$$\text{O}_2 = 7.941 \text{ gm cal/ gm mole } ^\circ\text{K}$$

$$\text{N}_2 = 7.507 \text{ gm cal/ gm mole } ^\circ\text{K}.$$

[16]

\*\*\*\*\*

FIRSTRANKER