

Code No: I2103/R16

M. Tech. I Semester Regular/Supple Examinations, Jan/Feb-2018

**ADVANCED HEAT AND MASS TRANSFER/
ADVANCED HEAT TRANSFER**

Common to Thermal Engineering (21) and Thermal Sciences And Energy Systems (18)

Time: 3 Hours

Max. Marks: 60

*Answer any FIVE Questions
All Questions Carry Equal Marks*

1. a What are Heisler charts? Explain its significance. [4]
b A short cylindrical aluminium bar, having thermal conductivity, 200W/m.K and thermal diffusivity, $8.4 \times 10^{-5} \text{ m}^2/\text{s}$ of diameter 6 cm and height 3 cm is initially at a uniform temperature of 175°C. Suddenly the surfaces are subjected to convective cooling with a heat transfer coefficient of 250 W/m².K into an ambient at 25°C. Calculate the center temperature of the cylinder one minute after the start of cooling. [8]
2. a Explain Dirichlet and Newmann Boundary conditions as applied to conduction with examples. [4]
b Write the finite difference form of the two dimensional steady state heat conduction equation with internal heat generation at a constant rate 'g' for a region 0.03m X 0.03m by using a mesh size $\Delta x = \Delta y = 0.01 \text{ m}$ for a material having thermal conductivity 25 W/m.K and heat generation rate, 10^7 W/m^3 . All the boundary surfaces are maintained at 10°C. Express the finite difference equations in matrix form for the unknown node temperatures. [8]
3. a Discuss the assumptions made in the Nusselts theory of film condensation on a vertical plate. [4]
b Prove that by using dimensional analysis Nusselt number is a function of Reynolds number and Prandtl number in forced convection. [8]
4. a Explain in detail, the differences between implicit and explicit methods. [4]
b By using approximate integral boundary layer analysis, derive the equation for the local heat transfer coefficient for the flow over flat plate in terms of the Reynolds number. [8]
5. a Explain and discuss the significance of (i) Rayleigh number and (ii) Nusselt number in natural convection. [4]
b Air at 20°C flowing at 25 m/s passes over a flat plate, the surface of which is maintained at 270°C. Calculate the rate at which heat is transferred from both the sides of the plate per unit width over a distance of 0.25 m from the leading edge. Properties of air at 145°C are Prandtl number = 0.687; Viscosity = $2.8 \times 10^{-5} \text{ m}^2/\text{s}$ and thermal conductivity = $3.49 \times 10^{-5} \text{ kW/m.K}$. [8]
6. a Write short notes on Gas radiation. [4]
b A 15 cm outer diameter steel pipe lies 2m vertically and 8 m horizontally in a large room with an ambient temperature of 30°C. If the pipe surface is at 250°C, calculate the total rate of heat loss from the pipe to the atmosphere. Properties of air at 140°C are density = 0.854 kg/m³; specific heat, $c_p = 1.01 \text{ kJ/kg.K}$; thermal conductivity = 0.035 W/m.K; Prandtl number = 0.684 and viscosity = $27.8 \times 10^{-6} \text{ m}^2/\text{s}$. [8]

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7. Draw the radiation network for a specular diffuse surface losing heat to a large enclosure. Obtain an expression for the heat transfer under these circumstances. How does this heat transfer compared with that which would be lost by a completely diffuse surface with the same emissivity. [12]
8. a Define Schmidt and Lewis numbers. Discuss the significances of each. [4]
b Assuming laminar film condensation, calculate the ratio of condensing heat transfer coefficient on a vertical tube to that of a horizontal tube of same diameter and length. [8]

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