

R09

Code: 9A23502

B.Tech III Year I Semester (R09) Supplementary Examinations, May 2013

BIOCHEMICAL REACTION ENGINEERING - I

(Biotechnology)

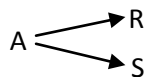
Time: 3 hours

Max. Marks: 70

Answer any FIVE questions
All questions carry equal marks

- 1 (a) Differentiate between elementary and non-elementary reactions.
(b) Differentiate between order and molecularity of reactions.
(c) The rate constant of a reaction at 27°C is $1.3 \times 10^{-3} \text{ s}^{-1}$. Determine the frequency factor. Take $E = 128170 \text{ cal/mol}$.
- 2 Using integral method of analysis show that $A+B \rightarrow \text{product}$ follows second order reaction. Assuming C_{A0}, C_{B0} initial concentrations of A and B respectively, $M = C_{B0}/C_{A0}$, initial molar ratio of reactants, C_A and C_B are concentrations of A and B at any time t .
- 3 Develop the performance equation of a PFR.
- 4 (a) Explain how the parameters are estimated in Monod's equation.
(b) Explain how sterilization is done in continuous mode.
- 5 Explain in detail about:
 - (a) Substrate inhibition kinetics.
 - (b) Product inhibition kinetics.

- 6 Liquid reactant A decomposes as per the following reaction scheme:



With rates: $r_R = K_1 C_A^2$, $K_1 = 0.4 \text{ m}^3/(\text{mol} \cdot \text{min})$

$r_S = K_2 C_A$, $K_2 = 2(\text{min})^{-1}$.

An aqueous feed containing A with $C_{A0} = 40 \text{ mol/m}^3$ enters a reactor, decomposes, and a mixture of A, R, S leave the reactor. Find the operating conditions (X_A, τ and C_R) which maximizes C_R in a mixed flow reactor.

- 7 Show that for non-adiabatic operation:

$$X_A = \frac{C_P \Delta T - Q}{-\Delta H R}$$

- 8 Explain in detail about the following:
 - (a) Dispersion model.
 - (b) Tanks-in-series model.
